Design of a Model-Following Controller with Stabilized Digital Inverse System in Closed Loop

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Abstract—In this paper, a design of a model-following controller with stabilized digital inverse system in a closed loop is proposed. In this paper, the proposed inverse system is placed in front of the plant. Our model-following control system was developed using the above structure. However, when the relative degree of the transfer function for a continuous-time plant is greater than 3, the discrete-time system is often in the non-minimum phase. In addition, unstable zeros appear when the chosen sampling period is too short. To solve these problems, an auxiliary output is used in the design. We designed a closed-loop system to consider the robustness of the proposed controller. In addition, a parallel feedforward compensator is added in parallel with the plant.

Index Terms—stabilized inverse system, multi-sampling rate, model-following control, parallel feedforward compensator

I. INTRODUCTION

In the industrial field, there are some plant inputs that cannot be used or are unknown. For example, they may be present in a complex plant or when an input signal is uncertain. Other examples include the effect of disturbances, age deterioration, saturation characteristics, trouble with equipments such as an actuator, and so on. These causes may not allow one to obtain a desired plant input.

Advanced techniques for estimating unpredictable disturbances have been proposed by some researchers, such as through the use of stabilized digital inverse systems [1]-[4]. By applying the inverse characteristic of the transfer function of the plant, reducing the influence of a disturbance is possible. The design for a stabilized digital inverse system was proposed by Kaku et al. [4]. They proposed a method for estimating an unknown disturbance by placing the inverse system after the plant. Kaku et al.’s method can be positioned at all poles so that the plant is stable even if it has a high order and is a non-minimum phase system. In particular, because of the existence of unstable limiting zeros and/or minimum phase property for continuous-time systems, there are many cases where discretized systems are in a non-minimum phase, thus, making it impossible to construct a stabilized digital inverse system by ordinary methods. To solve this problem, Kaku et al. have proposed a method of digital inverse system control designed using the observed output at a sample point and an auxiliary observed output between sample points.

On the basis of this method, we propose the design of a model-following controller using a digital inverse system to produce a stable closed-loop system. The auxiliary output adopted in the feedforward control is specifically designed for the proposed control system. First, even if the system has unstable or limited zeros when a continuous-time system is discretized, we can change the position of all zeros as required. Second, after calculating the unknown input of the plant, the inverse system is designed to operate in front of the plant. Third, we design a closed-loop system to consider the robustness of the proposed controller. In addition, a parallel feedforward compensator is added in parallel with the plant [5]-[10].

This paper is organized as follows. In Section 2, we describe a stable inverse system in the continuous-time domain. In Section 3, we describe a stable inverse system in the discrete-time domain of a closed-loop system. In section 4, the effectiveness of the method for two types of plants is confirmed by simulation results. Finally, in Section 5, we present the conclusion.

II. DESIGN OF A MODEL-FOLLOWING CONTROLLER WITH STABILIZED DIGITAL INVERSE SYSTEM

A continuous-time plant is expressed as

\[ \dot{x}(t) = A_c x(t) + b_c u(t) \]

(1a)

\[ y(t) = c_c x(t). \]

(1b)

With \( A_c \in \mathbb{R}^{n \times n} \), \( b_c \in \mathbb{R}^{n \times 1} \), and \( c_c \in \mathbb{R}^{1 \times n} \), where \( \dot{x}(t) \) is the differential of the state vector \( x(t) \), \( u(t) \) is the input, and \( y(t) \) is the output. The transfer function \( G_p(s) \) of Equation (1) from \( u(t) \) to \( y(t) \) is given by

\[ G_p(s) = c_c (sI_n - A_c)^{-1} b_c \]

(2)

where \( I_n \in \mathbb{R}^{n \times n} \) is an identity matrix.

The discrete-time system of Equation (1) with the sampling time \( T \) can be written as

\[ x_{i+1} = A_c x_i + b_c u_{mp} \]

(3a)

\[ y_i = c_c x_i. \]

(3b)

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where $\mathbf{x}_i = \mathbf{x}(iT)$, $\mathbf{y}_i = \mathbf{y}(iT)$, $A_d = e^{A_T}$, and $b_d = b_d \int_0^{iT} e^{A_T} dh$.

In the derivation of Equation (3), the input $u_{pi}$ is assumed to be constant over the sampling interval $iT \sim (i+1)T$. It is well known that $c_db_d \neq 0$ for almost all $T$ [2]. In this case, we can derive a simple inverse system with one delay, where the plant input $u_{pi}$ and state vector $x_{i+1}$ are expressed as

$$u_{pi} = (c_db_d)^{-1}(y_{i+1} - c_d A_d x_i) \quad (4a)$$

$$x_{i+1} = \left[A_d - b_d(c_db_d)^{-1}c_d A_d\right]x_i + b_d(c_db_d)^{-1}y_{i+1} \quad (4b)$$

However, the eigenvalues of $A_d - b_d(c_db_d)^{-1}c_d A_d$ are composed of the $n-1$ zeros of the discrete-time system of Equation (3) and zero located at the origin [11]. If the relative degree of the transfer function $G_m(s)$ is greater than 3 or the chosen sampling time $T$ is too short, the $n-1$ zeros include unstable ones. To solve this problem, an auxiliary output is designed

$$z_i = y(iT + mT), \quad (0 < m < 1) \quad (5)$$

That lags by $mT$ relative to the main sampling point $iT$, as shown in Fig. 1. The discrete-time system for the discrete-time model is written as

$$\mathbf{x}_{i+1} = \mathbf{A}_{md} \mathbf{x}_i + \mathbf{b}_{md} u_{pi}, \quad (6a)$$

$$\mathbf{y}_i = c_{md} \mathbf{x}_i, \quad (6b)$$

$$z_i = c_{md} \hat{\mathbf{A}}_{md} \mathbf{x}_i + c_{md} \hat{\mathbf{b}}_{md} u_{pi}, \quad (6c)$$

$$\mathbf{A}_{md} = e^{A_T}, \mathbf{b}_{md} = b_{md} \int_0^{iT} e^{A_T} dh, c_{md}. \quad (7)$$

where $(\mathbf{A}_{md}, \mathbf{b}_{md})$ are constant matrices of appropriate dimensions for the discrete-time model with sampling time $mT$ and can be written as

$$\hat{\mathbf{A}}_{md} = e^{A_{md}}, \mathbf{b}_{md} = b_{md} \int_0^{iT} e^{A_{md}} dh. \quad (8)$$

$$\hat{u}_{pi} = \left(c_db_d\right)^{-1} \left[z_i - c_d \hat{\mathbf{A}}_{md} \mathbf{x}_i\right]. \quad (9)$$

$$\hat{A}_d = e^{A_{md}}, \mathbf{b}_d = b_d \int_0^{iT} e^{A_{md}} dh. \quad (10)$$

where $(\hat{A}_d, \mathbf{b}_d)$ are constant matrices of appropriate dimensions for the discrete-time model with sampling time $mT$, when $c_d \mathbf{b}_d \neq 0$. In fact, the state vector $\mathbf{x}$ is estimated by an observer. Hence, Equation. (9) can be rewritten as

$$\hat{u}_{pi} = \left(c_db_d\right)^{-1} \left[z_i - c_d \hat{\mathbf{A}}_{md} \hat{\mathbf{x}}_i\right]. \quad (11)$$

where $\hat{\mathbf{x}}_i$ is an estimated state vector. Let a discrete-time state space expression for an observer be

$$\hat{x}_{i+1} = A_d \hat{x}_i + b_d \hat{u}_{pi} + L \left[y_i - \hat{y}_i\right] \quad (12a)$$

$$\hat{y}_i = c_d \hat{x}_i, \quad (12b)$$

where $L \in \mathbb{R}^{n 	imes 1}$ is observer gain solved by linear quadratic regulator, and $\hat{y}_i$ is estimated observer output. By substituting Equation (11) into Equation (12a), we obtain the following equation and Fig. 2:

$$\hat{x}_{i+1} = (A_d - Lc_d) \hat{x}_i + Ly_i + b_d \hat{u}_{pi} \quad (13)$$

The inverse system of Equations (11) and (13) may be stabilized despite the non-minimum phase properties of the discrete-time system. We design a model-following controller on the basis of the digital inverse system discussed in this section. In this controller, $y_i$ and $z_i$ are known inputs, and the plant input $\hat{u}_{pi}$ is an estimated inverse system output.

III. DESIGN OF A MODEL-FOLLOWING CONTROLLER WITH STABILIZED DIGITAL INVERSE SYSTEM IN A CLOSED LOOP

To consider its robustness, we design a closed-loop system. We reconfigure the model transfer function so that a closed-loop transfer function corresponds to the model transfer function. Therefore, the transfer function of the model $G_m(s)$ is given by

$$G_m(s) = \frac{\omega_n^2}{s^2 + 2\zeta\omega_n s + \omega_n^2} \quad (14)$$
where $\zeta$ and $\omega_n$ are arbitrary constants.

![Block diagram of proposed method.](image)

**IV. SIMULATION RESULTS**

In this section, the effectiveness of the proposed method is shown in simulations. An input is assumed as a step signal. A unit step set point is introduced at time $T = 0 \ [s]$. We consider two types of plants. They are discretized by the zero-order hold at the sampling time $T_s = 30 \ [ms]$, and we design the inverse system for continuous-time plants defined in Equation (1) when $m = 0.5$. The continuous-time zeros and the discrete-time zeros are defined to be the roots of

$$ (16a) \ \ \ c_n Adj(sI - A_x)b = 0, $$

$$ (16b) \ \ \ c_n Adj(sI - A_x)b = 0. $$

The equation (15) is the transfer function of the model. Damping coefficient is $\zeta = 1.0$. Natural angular frequency is $\omega = 10.0$.

**A. Case 1**

$$ G_{p1}(s) = \frac{s + 1}{s^2 + 2s + 2} \quad (17) $$

In this case, the continuous-time zero is $-1$ and discrete-time zero is $0.9704$. Therefore, the continuous-time system and discrete-time system have minimum phase properties.

The result of Case 1 is shown in Fig. 3

**B. Case 2**

$$ G_{p2}(s) = \frac{1}{s^2 + 6s^2 + 11s + 6}. \quad (18) $$

In this case, there is no continuous-time zero and the discrete-time zeros are $-3.5683$ and $-0.2561$. Therefore, the continuous-time system has a minimum phase property but the discrete-time system has a non-minimum phase property.

The result of Case 2 is shown in Fig. 4. Thus, from Fig. 3 and Fig. 4 we show that the plant output follows the model output.

![Result for case 1.](image)

**V. CONCLUSIONS**

In this paper, we proposed to design a model-following controller with stabilized digital inverse system in a closed loop. The inverse system is placed in front of the plant. In addition, an auxiliary observation inter-sample
output is adopted to stabilize the inverse system. Furthermore, the transfer function of the model is reconstructed so that the closed-loop transfer function corresponds to the model transfer function. In addition, a parallel feed-forward compensator is added in parallel with the plant. The effectiveness of the proposed method has been confirmed by simulation results in Section 4.

REFERENCES


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