

Design, Implementation and Evaluation of Fuzzy Logic and PID Controllers for Fuel Cell Systems

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Abstract—In this paper, fuel cell control is investigated in addition to the use of fuzzy logic to control fuel cells. For fuzzy rules, the maximum power point tracking algorithm is used. Additionally, PID control is used and tested in this paper. As simulation results show, the performance of fuzzy logic is better than PID control. In general, for fuel cell systems, humidification is required for the air or the hydrogen, or both the air and hydrogen at the fuel cell inlets. Moreover, water content is very important for the protonic conductivity in the proton exchange membranes. If membrane dehydration or drying occurs, electrical performance decreases due to significant ohmic losses.

Index Terms—fuel cell, fuzzy logic, PID controller

I. INTRODUCTION

Energy has been predicted as one of the main problems that humanity must face in the future. Nowadays, primary energy sources around the world consist of fossil fuels, namely petroleum, coal and natural gas. However, there are a number of problems with the continued use of fossil fuels. First, they are limited in amount and one day will be depleted. Secondly, they cause serious environmental problems such as global warming, climate change, acid rain, air pollution, ozone layer depletion, and so on. For these reasons, alternative energy sources are needed. These, in combination with fuel cells, make hydrogen energy systems a good alternative [1]. Hydrogen is a perfect energy carrier with its many unique properties. Together with hydrogen, fuel cells have been attracting much attention as they directly and efficiently convert the chemical energy of reactants into electrical energy. A fuel cell is an electrochemical device that converts the energy of chemical reactions directly into electrical energy by combining hydrogen with oxygen. In these chemical reactions, the only byproducts are heat and water. Fuel cells have many advantages over conventional systems that produce electricity, including and especially its higher efficiency than conventional systems.

Of the many types of fuel cells, Proton Exchange Membrane (PEM) fuel cells are spectacular due to their compactness, light weight, high power and low cost [1]. They have been noticed as the most promising power generating device candidates in portable electronic, automotive and distributed power generation applications

in the future [2]. In recent years, research into, and development activities relating to, fuel cells have accelerated. Although there are significant improvements in Proton Exchange Membrane technology, its performance, stability and reliability have not been sufficient to replace internal combustion engines. Moreover, the cost of fuel cell systems is still too high to become acceptable commercial products. The most important problems to be overcome are improvement of performance and cost reduction [3]. In PEM fuel cells, hydrogen and air humidification may be required in order to prevent the fuel cell membrane from dehydrating. At high current flows, there is ohmic heating that causes drying problems in the polymer membrane, which slows ionic transport through the membrane. Because of water generation on the air side in some fuel cell stacks, humidification is not required. Generally in fuel cell systems, humidification is required for either the air or hydrogen, or both the air and hydrogen at the fuel cell inlets. Water content is very important for the protonic conductivity in the proton exchange membranes. If membrane dehydration or drying occurs, electrical performance decreases due to significant ohmic losses [4]-[10]. In [11], the authors obtained a DC step-up gain that can make Microbial Fuel Cells (MFC) an Energy Aware Power Management Unit aimed arrays (EA-PMU) for an Inductor-less DC-DC (I-DCDC) converter that introduces efficient Maximum Power Point Tracking (MPPT). Because of identifying and selecting the best point of harvest time of the MFC's changing power profile, there is an increase in the efficiency and overall power distribution. Currently, the MFC series, or reverse voltage current issues with the MFC application, is limited due to parallel connections. This is a more reliable approach to harvest time multiplexing. However, upon leaving a new MFC harvest time each time, a new Maximum Power Point (MPP) is required. The recommended converter converts and maximizes efficiency as well as obtains the dynamic MPP which adapts in order to adjust their power consumption. Converters are designed and manufactured under a 0.18-micron CMOS process and they have an input power of 1.6mW, which shows 65% for maximum efficiency [11]. In [12], power optimization methods such as Maximum Power Point Tracking (MPPT) are applied to these cells using the systems. The Perturb and Observe (P & O) and Increasing Conductivity (IC) method for simulating is good for FC system applications which are compared to

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determine which [12]. In [13], the authors proposed a method for Wind Generator (WG) Maximum Power Point Tracking (MPPT) system, DC/DC converter and MPPT functions for control unit. The load impedance is matched with the impedance of the source under a given wind speed wind energy conversion system which can provide maximum strength. Because of the load and dynamically changing wind speed, Maximum Power Point Tracking (MPPT) becomes more complex. The advantages of the wind speed MPPT method, there is no need to measure WGA optimal power characteristic, and it can operate at variable speeds WGA. Thus, there is a system of high reliability, low complexity and less mechanical stress on the WG. In this paper, a hybrid algorithm is used for Maximum Power Point Tracking. In the author's method, the electrical variation and the duty cycle of the inverter output voltage are adjusted in accordance with various embodiments [13].

II. METHODOLOGY

A. The PID Controller

This controller replaces the amplifier in the forward path of our closed-loop control system. One example of PID controller is shown in Fig. 1.

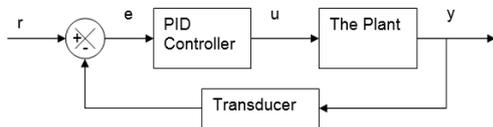


Figure 1. PID controller

“The Plant” merely refers to the equipment whose output is being controlled. In this figure, r is the reference input. We tell the system that we want the output y to settle at a value which will make the transducer output equal to y , where e is the error, u is the controller output or controller action and y is the plant output. We began our studies of such systems by using only an amplifier instead of the PID controller. The PID controller (also called a Three-Term Controller) actually incorporates what is effectively an amplifier. The output u of the PID controller is:

$$u = P \times e + I \times \int edt + D \times \frac{de}{dt} \quad (1)$$

where P , I and D are the Proportional, Integral and Derivative gains respectively. If I and D are both zero, the controller is just an amplifier with a gain P .

B. Modeling the System with Equations

A discrete PI controller is used as the fuel cell controller based on the following equation:

$$y(k) = y_p(k) + y_i(k) \quad (2)$$

where:

$$y_p(k) = K_p e(k)$$

$$y_i(k) = y_i(k-1) + K_i T_s e(k) \quad (3)$$

$$-1 \leq y_i(k) \leq 1$$

$y(k)$ - Controller output

$e(k)$ - Error (difference between desired output and actual output)

T_s - Sample time

K_p - Proportional gain

K_i - Integral gain

The Backward Euler method (a numerical integration approximation) is used to solve the integrator equation from above. This is why the integrator equation goes from $y_i(k-1)$ to $y_i(k)$.

The output of the integrator equation must fall between -1 and 1. This range is required as an anti-windup measure, or to prevent windup in the system. Windup refers to the condition when the controller is ineffective at reducing the system error, and so the integral state ($y_i(k)$) becomes very large. Table I shows the parameter of PID and their values that used in this paper.

TABLE I. THE PARAMETER USED IN THIS PROJECT IS AS BELOW

Parameter	Ki	Kd	Kp
Description	Integrator Coefficient	Derivative Coefficient	Proportional Coefficient
Value	100	0.1	30

C. Fuzzy Logic

Fuzzy logic is a theory that has been developed which colloquially refers to the modeling of uncertainty and vagueness of descriptions. It is a generalization of the divalent Boolean logic. For example, so-called fuzziness of information is “very” captured in mathematical models as “a bit,” “pretty” or “strong”. Fuzzy logic is based on fuzzy sets and so-called membership functions that represent objects in fuzzy sets and matches logic operations on these quantities and their inferences. Moreover, for technical applications, methods for fuzzification and defuzzification must be considered, that is, methods for the conversion of information and relationships in fuzzy logic and back again, such as a control value for a heater as a result. In Fig. 2, the fuzzy system is illustrated for a weather state.

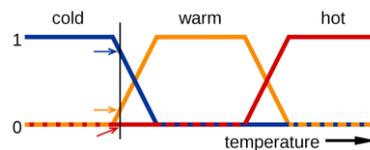


Figure 2. Fuzzy logic for weather state

This figure shows only three states. The other state is shown in Fig. 3.

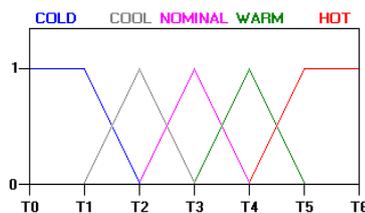


Figure 3. Fuzzy system for multistate for weather

For the PID controller, we used 5.28 for K_i , 1.32 for K_d , and for K_p we selected 5.28. These values were gained experimentally. The Simulink model that we used in our project is shown in Fig. 4.

logic controller is shown in Fig. 9. The flow rate of this stack is shown in Fig. 10.

In the saturation, we set the maximum value at 50, and the minimum value at 25. The fuel cell output power is shown in Fig. 11. As seen in this figure, after 12.5 seconds, the output is stable and fixed at 150.

Fig. 12 shows the efficiency of system. In this system, after an average time (after 12.5 sec), the system is stable with a value of 55 being obtained.

The fuel cell output power is shown in Fig. 13. As shown in this figure, the system after 15 seconds, produces 6000 (W) of power, which we selected as the parameter of stack. By reaching this value, we obtain the 6000 (W).

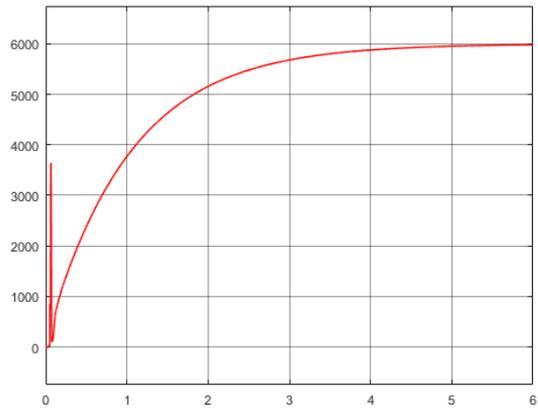


Figure 8. Simulation result for power

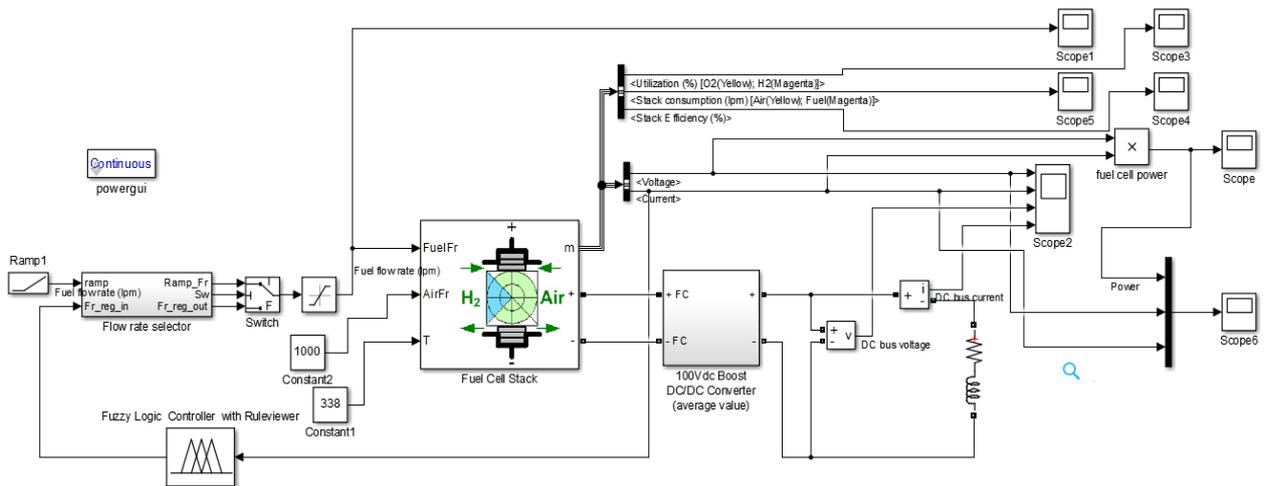


Figure 9. SIMULINK model used for Fuzzy logic

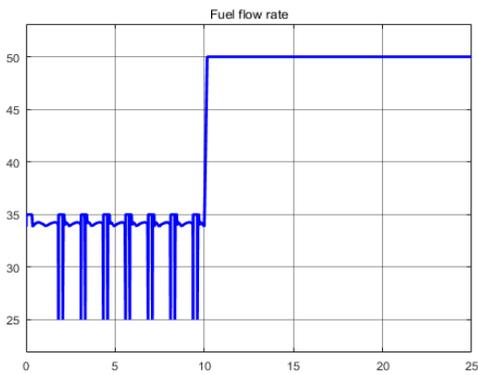


Figure 10. Flow rate of fuel cell stack

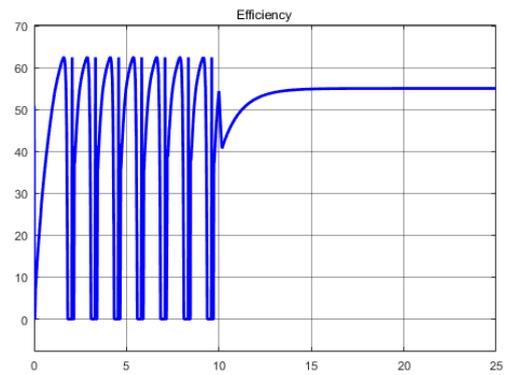


Figure 12. Efficiency of system

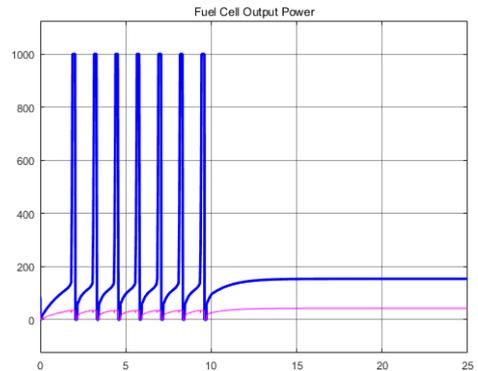


Figure 11. Fuel cell output power

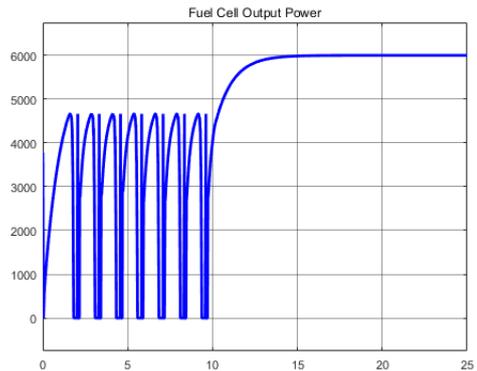


Figure 13. Fuel cell out put power 6000 watt

As shown in this figure, after 13 seconds, the final value for power is 6000 watts. The voltage curve, current, DC bus voltage and DC bus current is shown in Fig. 14. As shown in this figure, the voltage after the middle of the simulation time is stable, this value is 55 volt. For the current, this value is 0. Moreoever, for the DC bus voltage, the value is 100 volt and for the DC bus current we produce approximately 60A.

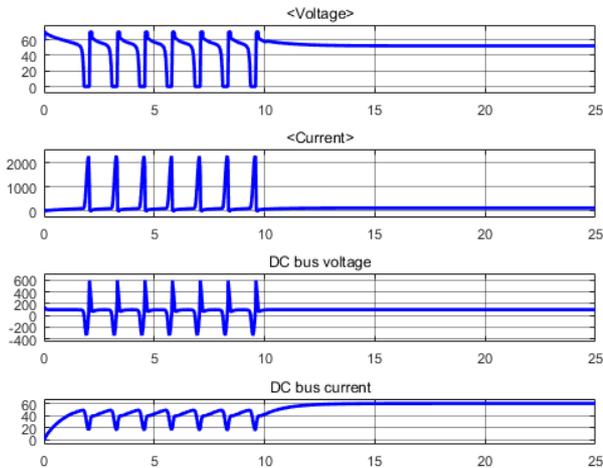


Figure 14. Voltage, current, DC bus voltage and DC bus current simulation result

The stack voltage vs current is shown in Fig. 15. As shown in this figure, this curve represents the value of voltage vs current. This simulation is inside the stack. For every current from 0A to 250A, the voltage is shown as below.

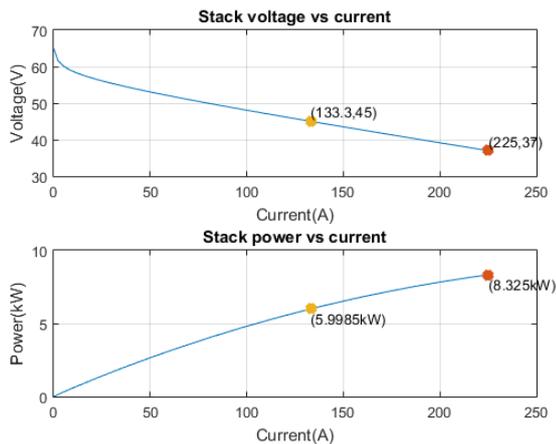


Figure 15. Stack voltage vs current and stack power vs current

Fig. 15 shows the stack power vs current. As seen in this figure the current start at 0A and increases 250A. The maximum power is 8.325KW.

The fuel cell nominal parameter is shown in Table II and Table III.

As shown in Table II, fuel cell resistance is 0.07833 ohms and the Nernst voltage of one cell is 1.1288 volts. For nominal utilization, there are two types of element, and these two types are the hydrogen and the oxidant. The Hydrogen takes approximately 99.56 percent of the material of the fuel cell, and the oxidant takes about 59.3 percent of this fuel cell. For nominal consumption, there are two elements, namely fuel and air. The exchange

current is 0.29197 Ampere and the exchange coefficient (alpha) is 0.60645 [14].

TABLE II. FUEL CELL NOMINAL PARAMETERS

Stack power	Nominal (w)	5998.5
	Maximal (w)	8325
Fuel Cell Resistance (ohms)	0.07833	
Nerst voltage of one cell [En] (V)	1.1288	
Nominal Utilization	Hydrogen (H ₂)	99.56 %
	Oxidant (O ₂)	59.3%
Nominal Consumption	Fuel (Slpm)	60.38
	Air (slpm)	143.7
Exchange current (A)	0.29197	
Exchange Coefficient [alpha]	0.60645	

TABLE III. FUEL CELL SIGNAL VARIATION PARAMETERS

Fuel composition (%)	99.95	
Oxidant Composition (%)	21	
Fuel flow rate (lpm)	Nominal	50.06
	Maximum	84.5
Air Flow Rate (lpm)	Nominal	300
	Maximum	506.4
System temperature (K)	338	
Fuel Supply Pressure (bar)	1.5	
Air supply pressure (bar)	1	

III. CONCLUSION

In recent years, research and development activities in fuel cells have accelerated. In spite of the significant improvements in the technology of proton exchange membranes, their performance, stability and reliability are not sufficient to replace internal combustion engines. Furthermore, the cost of fuel cell systems is still too high for them to become acceptable commercial products. The most important problems to be overcome are the improvement of their performance and the reduction of their cost. In PEM fuel cells, hydrogen and air humidification may be required in order to avoid fuel cell membrane dehydration. At high current flows, ohmic heating causes problems of drying in the polymer membrane and this slows ionic transport through the membrane. Due to water generation on the air side in some fuel cell stacks, humidification is not required. Generally in fuel cell systems, humidification is required for either the air or the hydrogen, or both the air and hydrogen at the fuel cell inlets. Water content is very important for the protonic conductivity in the proton exchange membranes. If membrane dehydration or drying occurs, electrical performance drops due to significant ohmic losses.

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